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Project Title :	**Bomboré Gold Project – Burkina Faso**		

TESTWORK REVIEW

FOR

BOMBORE GOLD PROJECT

FOR

OREZONE INC S.A.R.L.

(100% SUBSIDIARY OF OREZONE GOLD CORPORATION)

PREPARED BY

PROJECT NUMBER: 0379

14 OCTOBER 2009

Revision History

Rev	Date	Reason for Revision	By	Approved
A	21/09/09	Draft	AM	IJ
0	21/09/09	For Issue	AM	CB
1	12/10/09	Updated column test data incorporated	AM	LDT
2	13/10/09	Added comments on ADM and attached appendices	AM	LDT
3	14/10/09	Additions required for compliance with NI 43-101	AM	LDT

DISCLAIMER:

TABLE OF CONTENTS

LIST OF APPENDICES

This report was prepared as a National Instrument 43-101 Technical Report, in accordance with Form 43-101F1, for Orezone Gold Corporation by GBM Minerals Engineering Consultants Limited. The quality of information, conclusions, and estimates contained herein is based on:

i) information available at the time of preparation;

ii) data supplied by outside sources; and

iii) the assumptions, conditions, and qualifications set forth in this report.

This report is intended to be used by Orezone Gold Corporation, subject to the terms and conditions of its contract with GBM Minerals Engineering Consultants Limited. That contract permits Orezone Gold Corporation to file this report as a Technical Report with Canadian Securities Regulatory Authorities pursuant to provincial securities legislation. Except for the purposes legislated under provincial securities law, any other use of this report by any third party is at that party's sole risk.

This Technical Report describes the metallurgical results from a suite of samples from the Bomboré Gold Project, a mineral exploration and development area located in the Centre-Est Province of Burkina Faso. The Project is held by Orezone Inc., a British Virgin Island company owned at 100% by Orezone Gold Corporation.

The reader can refer to the NI 43-101 report filed by Orezone Gold Corporation in February 2009 for further information on the Bomboré Gold Project: "Technical Report on the Bomboré Gold Project in Burkina Faso, West Africa". Report prepared for Orezone Gold Corporation, 290 Picton Avenue, Suite 201, Ottawa, Ontario, Canada, K1Z 8P8 by SRK CONSULTING (CANADA) INC., Suite 1000, 25 Adelaide Street East, Toronto, Ontario, Canada, M5C 3A1.

SECTION 1 - INTRODUCTION

This report covers the testwork conducted by AMMTEC of Balcatta, Western Australia on ore from the Bomboré gold deposit on samples collected by Orezone Gold Corporation. The testwork procedures are shown in Appendix 1. Appendix 2 shows the Certificate of Qualification of the author of this report.

SECTION 2 - BOMBORE TESTWORK RESULTS

2.1 Physical Properties of the Ore

- Fresh ore moderately hard and abrasive:
  - Bond Work rod mill work index 19.5 kWh/tonne
  - Bond Work ball mill work index 16.8 kWh/tonne
  - Abrasion index 0.4064

- Transition ore soft and mildly abrasive:
  - Bond Work rod mill work index 7.8 kWh/tonne
  - Bond Work ball mill work index 8.2 kWh/tonne
  - Abrasion index 0.0383

- Oxide ore very soft and non abrasive:
  - Bond Work rod mill work index 5.4 kWh/tonne
  - Bond Work ball mill work index 1.9 kWh/tonne
  - Abrasion index 0.0051

2.2 Metallurgical Results

2.2.1 Bottle Roll Tests on Coarse Ore (test designed to assess viability of heap leaching)

- Fresh Ore Sample AM11
  - Extraction of 38.2% of the gold after crushing ore to < 4 mm

- Fresh Ore Sample AM12
  - Extraction of 43.8% of the gold after crushing ore to < 4 mm

- Transition Ore Sample AM21
  - Extraction of 72.5% of the gold after crushing ore to < 19 mm

- Transition Ore Sample AM22
  - Extraction of 72.4% of the gold after crushing ore to < 19 mm

- Oxide Ore Sample AM31
  - Extraction of 82.5% of the gold after crushing ore to < 25 mm

- Oxide Ore Sample AM32
  - Extraction of 84.2% of the gold after crushing ore to < 25 mm

2.2.2 Bottle Roll Tests on Milled Ore (test designed to determine recovery of gold by carbon in leach cyanidation)

- Fresh Ore Sample AM11
  - Extraction of 73.6% after milling ore to P_{80} of 53 µm and 8 hours leach time

- Fresh Ore Sample AM12
  - Extraction of 87.8% after milling ore to P_{80} of 53 µm and 8 hours leach time

- Transition Ore Sample AM21
  - Extraction of 90.9% after milling ore to P_{80} of 53 µm and 8 hours leach time

- Transition Ore Sample AM22
  - Extraction of 94.2% after milling ore to P_{80} of 53 µm and 8 hours leach time

- Oxide Ore Sample AM31
  - Extraction of 92.4% after milling ore to P_{80} of 53 µm and 8 hours leach time

- Oxide Ore Sample AM32
  - Extraction of 94.8% after milling ore to P_{80} of 53 µm and 8 hours leach time

2.2.3 Flotation/Leaching Tests on Milled Ore (test designed primarily to attempt to improve recovery from fresh ore)

- Fresh Ore Sample AM11
  - Float recovery of 92.4% in 11.4% of feed mass from ore milled to P_{80} of 53 µm; leaching concentrate extracted 77.9% to give an overall gold recovery of 71.8%
- Fresh Ore Sample AM12
  - Float recovery of 85.0% in 7.4% of feed mass from ore milled to P80 of 53 µm; leaching the concentrate extracted 86.9% to give an overall gold recovery of 73.9%
- Transition Ore Sample AM21
  - Gold recovery of 69.9% by floating ore milled to P80 of 75 µm
- Transition Ore Sample AM22
  - Gold recovery of 69.7% by floating ore milled to P80 of 75 µm
- Oxide Ore Sample AM31
  - Gold recovery of 65.0% by floating ore milled to P80 of 75 µm
- Oxide Ore Sample AM32
  - Gold recovery of 67.2% by floating ore milled to P80 of 75 µm

2.2.4 Gravity Concentration with Leaching of Gravity Tailings (test designed to determine effect of gravity concentration)

- Fresh Ore Sample AM11
  - Gravity gold recovery of 14.2%, additional recovery by leaching gravity tailings 49.0% to give overall recovery of 63.2%
- Fresh Ore Sample AM12
  - Gravity gold recovery of 17.6%, additional recovery by leaching gravity tailings 65.5% to give overall recovery of 83.1%
- Transition Ore Sample AM21
  - Gravity gold recovery of 12.2%, additional recovery by leaching gravity tailings 73.3% to give overall recovery of 85.4%
- Transition Ore Sample AM22
  - Gravity gold recovery of 20.7%, additional recovery by leaching gravity tailings 69.2% to give overall recovery of 89.9%
- Oxide Ore Sample AM31
  - Gravity gold recovery of 9.3%, additional recovery by leaching gravity tailings 76.9% to give overall recovery of 86.2%
- Oxide Ore Sample AM32
  - Gravity gold recovery of 7.2%, additional recovery by leaching gravity tailings 71.8% to give overall recovery of 79.0%

2.2.5 Column Leaching (test designed to confirm results of coarse ore bottle roll tests and to generate data for design of a heap leach operation)

Given the poor results of coarse bottle tests on fresh ore, only the oxide and transition ore were selected for column leaching.

- Transition Ore Sample AM21
  - Indicated gold recovery of 76.0% after 26 days of leaching
- Transition Ore Sample AM22
  - Indicated gold recovery of 84.1% after 26 days of leaching
- Oxide Ore Sample AM31
  - Indicated gold recovery of 80.4% after 26 days of leaching
- Oxide Ore Sample AM32
  - Indicated gold recovery of 78.8% after 26 days of leaching

2.3 Acid Mine Drainage (AMD) Tests

These tests were performed to determine the likelihood of acid generation from products from mining and processing. The propensity of a material to produce acid is related to amount of sulphide sulphur present. The sulphidic material undergoes wet oxidation to form sulphuric acid according to reaction:

$$2S^{-2} + 3O_2 + 2H_2O = 2H_2SO_4$$

The elements of the AMD tests are:

- Sulphur Assay
  - AM11- Total sulphur 3.23%, sulphide sulphur 2.93%
  - AM12- Total sulphur 1.79%, sulphide sulphur 1.46%
  - AM21- Total sulphur 0.22%, sulphide sulphur 0.08%
  - AM22- Total sulphur 0.06%, sulphide sulphur 0.03%
  - AM31- Total sulphur 0.12%, sulphide sulphur <0.02%
  - AM32- Total sulphur 0.03%, sulphide sulphur <0.02%
- ANC (Acid Neutralizing Capacity). This is a measure of the capacity of minerals present in the ore (e.g. carbonates) to neutralise any acid produced by wet oxidation.
  - AM11- 97.3 kg H2SO4/tonne of ore
  - AM12- 75.9 kg H2SO4/tonne of ore
  - AM21- 23.6 kg H2SO4/tonne of ore
  - AM22- 10.0 kg H2SO4/tonne of ore
  - AM31- 8.22 kg H2SO4/tonne of ore
  - AM32- 79.5 kg H2SO4/tonne of ore
- NAG (Net Acid Generation). This is a measure of the actual net acid produced by the ore under powerful oxidizing conditions produced by use of hydrogen peroxide and heat. A negative figure indicates that neutralizing capacity of the ore exceeds its ability to produce acid.
  - AM11- minus 10.3 kg H2SO4/tonne of ore
  - AM12- minus 9.43 kg H2SO4/tonne of ore
  - AM21- minus 10.4 kg H2SO4/tonne of ore

- AM22- minus 6.11kg H2SO4/tonne of ore
- AM31- minus 7.38 kg H2SO4/tonne of ore
- AM32- minus 5.26 kg H2SO4/tonne of ore

- TAPP (Total Acid Production Potential). This is a calculated figure based on the total sulphur assay. Some laboratories the sulphide sulphur assay which would give a lower figure.
  - AM11- 98.52 kg H2SO4/tonne of ore
  - AM12- 54.60 kg H2SO4/tonne of ore
  - AM21- 6.71 kg H2SO4/tonne of ore
  - AM22- 1.83 kg H2SO4/tonne of ore
  - AM31- 3.66 kg H2SO4/tonne of ore
  - AM32- 0.92 kg H2SO4/tonne of ore

- NAPP (Net Acid Production Potential). This is a calculated figure obtained by subtracting ANC from TAPP and represents the worst case scenario.
  - AM11- 1.25 kg H2SO4/tonne of ore
  - AM12- minus 21.32 kg H2SO4/tonne of ore
  - AM21- minus 16.88 kg H2SO4/tonne of ore
  - AM22- minus 8.19kg H2SO4/tonne of ore
  - AM31- minus 4.56 kg H2SO4/tonne of ore
  - AM32- minus 7.03 kg H2SO4/tonne of ore

- pH and Conductivity Measurements. These measurements were taken in the NAG tests, the latter can give an indication of the inherent salinity of the solution.
  - AM11- pH 6.27, conductivity 1.502 mS/cm
  - AM12- pH 4.76, conductivity 1.137 mS/cm
  - AM21- pH 6.17, conductivity 0.26 mS/cm
  - AM22- pH 3.92, conductivity 0.202 mS/cm
  - AM31- pH 3.99, conductivity 0.179 mS/cm
  - AM22- pH 3.80, conductivity 0.18 mS/cm

2.4 Comments

It is evident that Carbon in Leach (CIL) cyanidation gives the optimum recovery from oxide and transition ore samples, extractions of 90+% being obtained from oxide and transition ore samples. The result from fresh ore of the type represented by sample AM12 with an extraction of at 87.8% is slightly poorer and that from sample AM11 is some 14% lower at 73.6%. A higher recovery of 92.4% was obtained from sample AM11 by flotation but the flotation concentrate would require some additional treatment to produce bullion. With a high grade ore, bio-leaching or pressure leaching could be considered but, with this low grade material, only leaching after very fine grinding provides the possibility of an economical solution. When this approach was used, leaching of the flotation concentrate after grinding to 11 µm only extracted 77.9% of the gold in the concentrate giving an overall recovery of 71.8%, slightly lower than obtained by CIL.

With a high grade deposit, a probable approach would be to use CIL leaching for the oxide and transition ores with the possibility of a later addition of flotation followed by bio-leaching or pressure leaching if this proved economically viable. However, the Bomboré deposit is not high grade and could not support, at least for the oxide and transition ore with grades of about 0.5 g/t, a process requiring ore to be milled to a P_{80} of 53 µm.

Coarse bottle roll tests on the oxide and transition ores showed extractions of about 83% and 72% respectively, some 10 to 20% lower than CIL. Column leaching tests to confirm the results of the bottle roll tests are underway and after twenty six days of leaching, results from the transition ore at 76.0% for sample AM 21 and 84.1% for AM 22 are exceeding the expectations based on coarse bottle roll tests. The curve of recovery versus time for these samples indicates that extraction of gold is not yet complete but only a moderate increase in recovery can be expected as the test continues over time. In case of the oxide samples, results from the column tests at 80.4% and 78.8% for samples AM31 and AM32 respectively are some 3.5% lower than observed from the coarse bottle tests and further, the curve of recovery versus time for these samples indicates that extraction of gold from AM 32 is almost complete and little increase in recovery can be expected but a moderate increase in extraction can still be expected from AM31. Nevertheless, an average extraction of about 80% from both ore types in a comparatively short time shows the ores to be very amenable to heap leaching. These reported extractions are based on assays of the solution leaving the column and thus are only indicative of the leaching results; the final figure will only be obtained when leaching appears to be complete and the leach residue is removed from the column for assay.

Comparing average results of CIL (93.6% for oxide ore and 92.6% for transition ore) and the 26 day column leach results (79.6% for oxide ore and 80.0% from the transition ore), heap leaching oxide and transition ores will result in a 14.0% and 12.6% loss in recovery respectively. Reductions in recovery of these magnitudes from a 0.5 g/t ore represent gold losses of 0.070g/t by heap leaching oxide ore and 0.063g/t by heap leaching oxide transition ore. At gold price of US$1000/oz or US$32.62/g, this would result in a loss in revenue of US$2.28/tonne treated for oxide ore and US$2.06/tonne treated for transition ore. As of day 26, the cyanide consumption indicated by column leaching of the transition samples AM21 and AM22 was 0.44 kg/t and 0.55 kg/t respectively. In the case of the oxide samples AM31 and AM32, cyanide consumption was 0.29 kg/t and 0.44 kg/t respectively. The lime consumption was 0.52 kg/t for all samples except AM31, where it was 0.50 kg/t. Applying the averages of these consumption figures, an operating cost of US$5.95/t for processing transition ore and US$7.38/t for processing oxide ore can be determined. These costs include reagents, labour, engineering and power. These costs contrast with the operating cost of a milling/CIL operation, which be expected to be in the range of US$10-12/tonne treated for a 3 Mtpa operation. In addition, the capital cost of such a milling/CIL operation would be significantly higher than that of a heap leaching operation.

In the case of the fresh ore, the loss in recovery is of the order of 40% and the fresh ore at 0.84 g/t is higher grade so the loss in revenue by use of heap leaching as opposed to CIL would be about US$11/tonne treated thus, in terms of operating cost, CIL would be favoured but even so, the capital expenditure for a CIL plant might not be economically justifiable.

The results from gravity concentration with CIL leaching of the gravity tails were poorer than those obtained by CIL alone; in the case of sample AM32, the result was even worse than that obtained in the coarse bottle test. There is no logical explanation for these poorer results and the testing facility could offer no explanation. The leach residues were re-assayed with similar results being obtained. Accordingly, these results should be

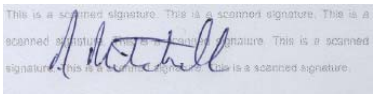
considered suspect but since heap leaching is the indicated processing approach, further investigation is probably of only academic interest.

The results of the AMD tests indicate that acid mine drainage will not be a problem as neutralizing capacity of the ore exceeds its ability to produce acid.

SECTION 3 - REPORT SIGNOFF

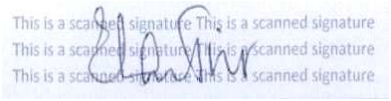
The following were involved in the completion of this report.

Prepared By :



Alex Mitchell (GBM MEC Ltd)

Reviewed By :

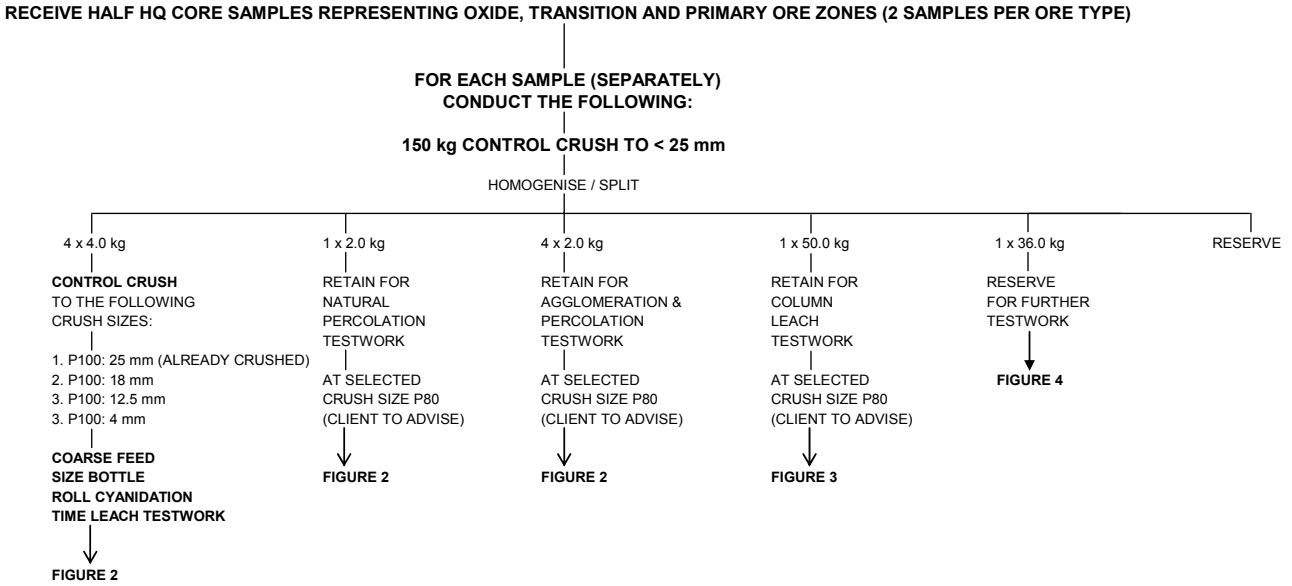


Ludwig du Toit (GBM MEC Ltd)

Appendix 1 : Testwork Procedures

FIGURE 1 : COARSE SAMPLE PREPARATION & PRELIMINARY TESTWORK

BOMBORE GOLD PROJECT : OREZONE GOLD CORPORATION



NOTE : USE PERTH TAP WATER FOR ALL TESTWORK UNLESS SITE WATER PROVIDED

FIGURE 2 : COARSE BOTTLE ROLL LEACH & AGGLOMERATION TESTS

BOMBORE GOLD PROJECT : OREZONE GOLD CORPORATION

FOR EACH SAMPLE (SEPARATELY) - CONDUCT THE FOLLOWING:

COARSE CRUSHED SUB-SAMPLES FROM FIGURE 1

4 x 4.0 kg

COARSE FEED SIZE BOTTLE ROLL CYANIDATION TIME LEACH TESTWORK @ FOLLOWING CRUSH SIZES :
1] 100% < 25 mm
2] 100% < 18 mm
3] 100% < 12.5 mm
4] 100% < 4 mm

* 40% SOLIDS (w/w)
* pH : 10.5 [LIME]
  MAINTAIN pH > 9.5
* NaCN : 0.10% (w/v)
  MAINTAIN NaCN > 0.05%
* DURATION : 144 HOURS
* INTERMITTENT ROLL AGITATION :
  1 MINUTE PER HOUR OF LEACH CONTACT
* SAMPLE @ 2, 4, 8, 24, 48, 72, 96, 120 & 144 HOURS
* MONITOR pH, DO & NaCN LEVELS.
* ANALYSE LEACH SOLUTIONS : Au, Cu
* ANALYSE LEACH RESIDUE : Au, Cu
* RETAIN 2.0kg OF RESIDUE FOR SIZE BY SIZE GOLD ANALYSIS (CLIENT TO ADVISE)

→ *DETERMINE OPTIMUM CRUSH SIZE FOR COLUMN CYANIDATION LEACH TESTWORK [CLIENT TO ADVISE]*

1 x 2.0 kg

CONDUCT NATURAL PERCOLATION TESTWORK

AT SELECTED CRUSH SIZE P80 (CLIENT TO ADVISE)

DETERMINE IF AGGLOMERATION IS REQUIRED

4 x 2.0 kg

CONDUCT AGGLOMERATION & PERCOLATION TESTWORK

AT SELECTED CRUSH SIZE P80 (CLIENT TO ADVISE)

TESTWORK @ FOLLOWING CEMENT DOSAGES :
1] 2.0kg/t
2] 5.0kg/t
3] 10.0kg/t
WITH LIME @ 10kg/t

* CURING PERIOD : 24 HOURS
* CONDUCT PERCOLATION RATE TESTWORK
* DETERMINE SLUMPAGE

DETERMINE OPTIMUM CEMENT DOSAGE [CLIENT TO ADVISE]

RESERVE

NOTE : USE PERTH TAP WATER FOR ALL TESTWORK UNLESS SITE WATER PROVIDED

FIGURE 3 : COLUMN LEACH TESTWORK

BOMBORE GOLD PROJECT : OREZONE GOLD CORPORATION

CONVENTIONAL CRUSHED SAMPLE @ SELECTED P100 CRUSH SIZE (FROM FIGURE 2)

1 x 50 kg

RESERVE

PREPARE SAMPLE AT AS REC'D CRUSH SIZE
AGGLOMERATE WITH CEMENT IF REQUIRED

LOAD SAMPLE INTO 20cm DIAMETER TRANSPARENT COLUMN
MEASURE HEIGHT OF SAMPLE FOR SLUMPAGE DETERMINATION

FEED COLUMN 8.0 LITRES OF pH 10.0 / 0.05% NaCN SOLUTION DAILY
RECYCLE LIQUOR TO BE MAINTAINED AT ABOVE LEVELS ON A DAILY BASIS

COLUMN CYANIDATION LEACH TESTWORK
* DURATION : 60 DAYS (8 WEEKS)
  [CLIENT TO ADVISE ON TERMINATION TIME]
* ANALYSE PREG. LIQUOR DAILY :
  Au, Cu, SG, pH, NaCN SOLUTION STRENGTH,SOLUTION VOLUME
* PASS LIQUOR THROUGH CARBON
  CONTACT STAGE
* ANALYSE BARREN LIQUOR :
  Au, Cu, SG, pH, NaCN SOLUTION STRENGTH,SOLUTION VOLUME
* ANALYSE CARBON : Au, Cu
* CONDUCT 7 x WASH CYCLES
  @ TERMINATION
* ANALYSE WASH LIQUOR :
  Au, Cu, SG, pH, NaCN SOLUTION STRENGTH,SOLUTION VOLUME
* MEASURE PERCOLATION RATE
* MEASURE SLUMPAGE
* EMPTY COLUMN IN 1/4 LENGTHS
* SPLIT EACH 1/4 LENGTH OF LEACH RESIDUE
* ANALYSE 4 x RESIDUES : Au, Cu
* CONDUCT SIZE BY SIZE ANALYSIS ON LEACH RESIDUE - OVER 8 SCREEN FRACTIONS
* ALL SIZE BY SIZE ANALYSIS SCREEN FRACTIONS - SCREEN FIRE ASSAY FOR : Au, Cu

Photographs to be taken for column leach test

NOTE : USE PERTH TAP WATER FOR ALL TESTWORK UNLESS SITE WATER PROVIDED

FIGURE 4 : GRAVITY, CYANIDATION & FLOTATION TESTWORK

BOMBORE GOLD PROJECT : OREZONE GOLD CORPORATION

FOR EACH SAMPLE (SEPARATELY)
CONDUCT THE FOLLOWING:

CONTROL CRUSH 36 kg TO < 3.35mm

HOMOGENISE / SPLIT

1 x 0.5 kg

HEAD ASSAY
FOR:
Au, Ag, As,
Cu, Fe,
S total
S sulphide
C total
C organic
ICP Scan

CONDUCT
TRUE SG
DETERMINATION

AMD TESTING:
ANC
NAG
TAPP
NAPP

3 x 1 kg

GRIND ESTABLISHMENT

CONDUCT TRIAL GRINDS
TO DETERMINE TIME
REQUIRED TO ACHIEVE
P80's of 150, 106, 75 & 53 µm

4 x 1 kg

CARBON IN LEACH TESTS

GRIND 1 kg ORE TO EACH OF
P80's of 150, 106, 75 & 53 µm

LEACH TESTING

* 40% SOLIDS (w/w)
* pH : 10.5 [LIME]
  MAINTAIN pH > 9.5
* NaCN : 0.10% (w/v)
  MAINTAIN NaCN > 0.05%
* ADD 50 g OF ACTIVATED CARBON
* OXYGEN SPARGE
* DURATION : 48 HOURS
* CONTINUOUS ROLL
  AGITATION :
* SAMPLE SOLUTION &
  CARBON @ 2, 4, 8, 24 & 48 HOURS
* MONITOR pH, DO &
  NaCN LEVELS.
* ANALYSE LEACH
  SOLUTIONS : Au, Cu
* ANALYSE CARBON
  SAMPLES : Au, Cu
* ANALYSE LEACH
  RESIDUE : Au, Cu
* RETAIN 0.5 kg OF RESIDUE FOR
  SIZE BY SIZE GOLD ANALYSIS
(CLIENT TO ADVISE)

3 x 1 kg

GRIND TO OPTIMUM SIZE

KNELSON CONCENTRATOR TEST

RECOVER KNELSON CONCENTRATE
AMALGAMATE, ASSAY FOR Au

COMBINE AMAGAM TAIL
AND KNELSON TAIL

LEACH TESTING

* 40% SOLIDS (w/w)
* pH : 10.5 [LIME]
  MAINTAIN pH > 9.5
* NaCN : 0.10% (w/v)
  MAINTAIN NaCN > 0.05%
* ADD 50 g OF ACTIVATED CARBON
* OXYGEN SPARGE
* DURATION : 48 HOURS
* CONTINUOUS ROLL
  AGITATION :
* SAMPLE SOLUTION &
  CARBON @ 2, 4, 8, 24 & 48 HOURS
* MONITOR pH, DO &
  NaCN LEVELS.
* ANALYSE LEACH
  SOLUTIONS : Au, Cu
* ANALYSE CARBON
  SAMPLES : Au, Cu
* ANALYSE LEACH
  RESIDUE : Au, Cu
* RETAIN 0.5 kg OF RESIDUE FOR
  SIZE BY SIZE GOLD ANALYSIS
(CLIENT TO ADVISE)

4 x 1 kg

FLOTATION TESTS

GRIND 1 kg ORE TO EACH OF
P80's of 150, 106, 75 & 53 µm

FLOTATION TESTING

* 30% SOLIDS (w/w)
* pH : NATURAL

* XANTHATE & AEROPROMOTOR (t.b.a)
* COLLECT 4 CONCENTRATES
* SPLIT CONCENTRATES FOR ASSAY & RETAIN BALANCE
* ANALYSE CONS & SCAVENGER
  TAIL : Au, Cu, S
* RETAIN 0.5 kg OF TAILS FOR
  SIZE BY SIZE GOLD ANALYSIS
  OR FOR CYANIDATION TESTING
(CLIENT TO ADVISE)

COMBINE CONCENTRATE RESERVES FROM OPTIMUM TEST

UFG CONCENTRATE (NOMINAL GRIND) - CHECK LASER SIZING

48HR INTENSIVE CIL
CYANIDATION LEACH TESTWORK

* 25% SOLIDS (w/w)
* pH : 10.5 [Lime], MAINTAIN pH >9.8
* NaCN : 0.5% (w/v), MAINTAIN >0.4%
* ADD 100g/L OF CARBON
* OXYGEN SPARGE
* DURATION : 48 HOURS
* ANALYSE SOLUTION,
CARBON & RESIDUE:
Au, Cu.

RESERVE
FOR FURTHER
TESTWORK

ANNTEC Ltd

FIGURE 5 : COMMINUTION TEST PROGRAMME FLOWSHEET - ***FULL SAG MILL TESTWORK***

OREZONE GOLD CORPORATION / GBM MINERALS ENGINEERING CONSULTANTS : BOMBORE GOLD PROJECT

TRANSITION ORE BULK SAMPLE OF WHOLE PQ CORE [80mm diameter] : 300kg REQUIRED
PRIMARY ORE BULK SAMPLE OF WHOLE PQ CORE [80mm diameter] : 300kg REQUIRED

CONDUCT THE FOLLOWING ON EACH SAMPLE SEPARATELY

UNCONFINED COMPRESSIVE STRENGTH (UCS) TESTS :
ON SELECTED
SPECIMENS [5 TESTS]

BOND IMPACT CRUSHING WORK INDEX DETERMINATION
ON SELECTED
SPECIMENS [10]

MEDIA COMPETENCY TESTWORK
1 x 180kg OF WHOLE PQ CORE [UN-BROKEN CYLINDERS]

CONDUCT BOND IMPACT CRUSHING WORK INDEX
TESTS ON 20 PIECES FROM
5 x DIFFERENT SIZE RANGES
FROM THE MEDIA COMPETENCY
TEST PRODUCTS (100 CWi's IN TOTAL)
-89+76mm
-76+51mm
--51+38mm
-38+25mm
-25+19mm

CONTROL CRUSH THE REMAINDER TO < 63.0mm

HOMOGENISE & SPLIT

1 x 10.0 Kg
SCREEN @ :
-55.0+38.0mm
2 x 3.0 Kg
SUB-SAMPLES
CONDUCT JK ABRASION TESTWORK
[t_a]

1 x 60.0 Kg
SCREEN @ :
53.0mm
37.5mm
26.5mm
19.0mm
13.2mm
SELECT 4 x 10
PARTICLES
SUITE EX :
-63.0+53.0mm
SELECT 4 x 15
PARTICLES
SUITE EX :
-45.0+37.5mm
SELECT 4 x 30
PARTICLES
SUITES EX :
-31.5+26.5mm
-22.4+19.0mm
-16.0+13.2mm
CONDUCT JK DROP-WEIGHT TESTS @ 3 ENERGY LEVELS PER SIZE RANGE
RELAY DATA TO JK TECH
FOR THE EVALUATION
OF FAG/SAG MILL PARAMETERS [A, b]

1 x 20 Kg
CONTROL CRUSH
TO < 31.5mm
SELECT 2 x 30
PARTICLES
SUITE EX :
-31.5+26.5mm
CONDUCT APPARENT SG DETERMINATIONS AS PART OF JK DROP-WEIGHT TESTWORK

1 x 30kg
CONTROL CRUSH TO < 20mm
HOMOGENISE & SPLIT

1 x 5.0 Kg
CONTROL CRUSH
TO < 20.0 mm
SCREEN @ :
-19.0+12.7mm
SELECT 4 x 400 g
SUB-SAMPLES
CONDUCT BOND ABRASION INDEX DETERMINATION
[Ai]

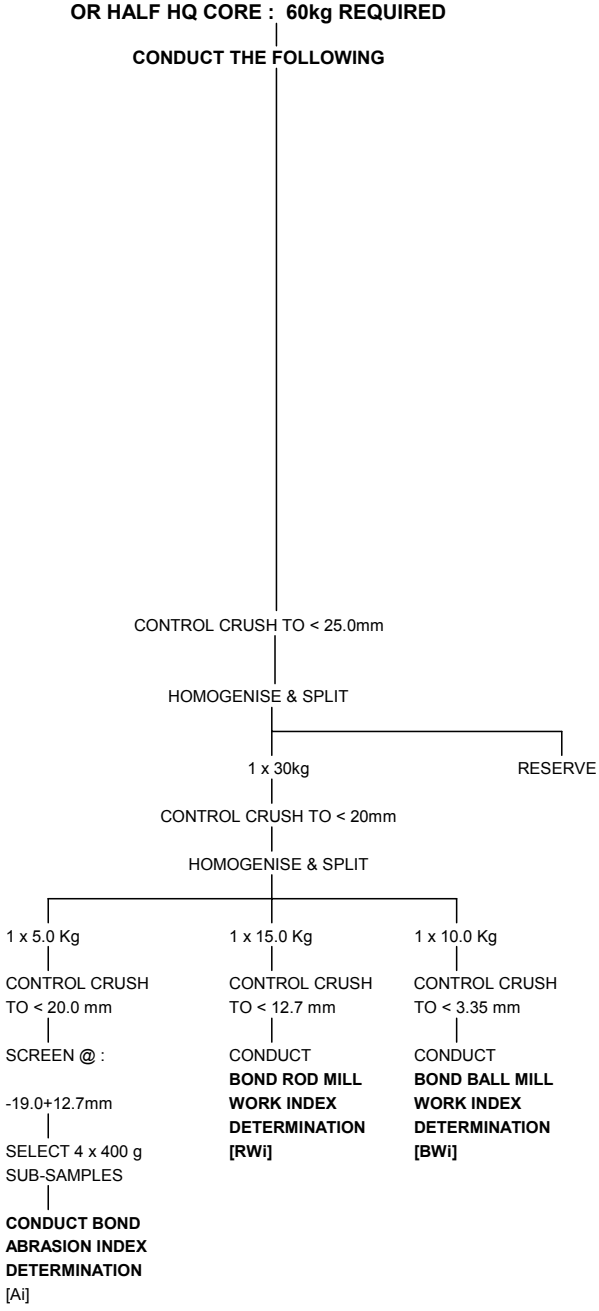
1 x 15.0 Kg
CONTROL CRUSH
TO < 12.7 mm
CONDUCT
BOND ROD MILL WORK INDEX DETERMINATION
[RWi]

1 x 10.0 Kg
CONTROL CRUSH
TO < 3.35 mm
CONDUCT
BOND BALL MILL WORK INDEX DETERMINATION
[BWi]

RESERVE

FIGURE 6 : COMMINUTION TEST PROGRAMME FLOWSHEET - PHYSICAL ***TESTWORK***

OREZONE GOLD CORPORATION / GBM MINERALS ENGINEERING CONSULTANTS : BOMBORE GOLD PROJECT



Appendix 2 : Certificate of Qualification

CERTIFICATE OF QUALIFICATION

Alex Mitchell, C.Eng
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England

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Fax: +44 20 8607 9777
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CERTIFICATE OF AUTHOR

I, Alex Mitchell, C.Eng, do hereby certify that:

1. I am the Principal Metallurgist with GBM MEC Ltd, Regal House, 70 London Road, Twickenham, Middlesex TW1 3QS, England;
2. I graduated with an honours degree in Applied Chemistry from Heriot-Watt University in Edinburgh, Scotland;
3. I am a member in good standing of the Institute of Materials, Minerals and Mining (formerly the Institution of Mining and Metallurgy), membership number 42939;
4. I have worked continuously as a metallurgist worldwide in operating and consulting roles since 1966;
5. I have read the definition of "qualified person" set out in National Instrument 43-101 (NI 43-101) and certify that by reason of my education, affiliation with a professional association (as defined by NI 43-101) and past relevant work experience, I fulfil the requirements to be a "qualified person" for the purposes of NI 43-101;
6. I am responsible for the preparation of the report entitled "Testwork Review for Bomboré Gold Project" and dated 13 October 2009 (the Technical Report) relating to a testwork program, designed and monitored by me but conducted in the testing facility of AMMTEC, Balcatta, Western Australia;
7. I have not visited the Bomboré project site;
8. I am not aware of any material fact or material change with respect to the subject matter of the Technical Report, which is not reflected in the Technical Report, the omission to disclose which makes the Technical Report misleading;

9. I am independent of the issues as defined in Section 1.4 of NI 43-101;

10. I have read National Instrument 43-101 and Form 43-101F1, and the Technical Report has been prepared in compliance with that instrument and form;

11. I consent to the filing of the Technical Report with any Canadian stock exchange and other securities regulatory authority and any publication by them for regulatory purposes of the Technical Report.

This 13th day of October 2009

Alex Mitchell, C.Eng
Principal Metallurgist
GBM MEC Ltd

GBM

Consultants Engineers Constructors

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CONSENT OF EXPERT

To: Ontario Securities Commission (Principal Regulator)
British Columbia Securities Commission
Alberta Securities Commission
Saskatchewan Financial Services Commission, Securities Division
The Manitoba Securities Commission
Autorité des marchés financiers
New Brunswick Securities Commission
Nova Scotia Securities Commission
Prince Edward Island Securities Office
Securities Commission of Newfoundland and Labrador
Yukon Registrar of Securities
Northwest Territories Registrar of Securities
Nunavut Registrar of Securities

Dear Sirs / Mesdames

Re: Orezone Gold Corporation (the "Company")
"Testwork Review for Bomboré Gold Project" dated 13 October 2009 (the "Report")

The undersigned hereby consents to the filing of the Report, prepared for the Company, with the securities regulatory authorities referred to above. The undersigned further consents to the filing of the Report with any stock exchange and other regulatory authority and any publication of the Report by them for regulatory purposes.

Dated this 13th day of October 2009

Alex Mitchell, C.Eng
Principal Metallurgist